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U.S. Department of Commerce Patent and Trademark Office

ATTORNEY'S DOCKET NO.

1101.104US01

TRANSMITTAL LETTER TO THE UNITED STATES
DESIGNATED/ELECTED OFFICE (DO/EO/US)
CONCERNING A FILING UNDER 35 U.S.C. 371

US APPLICATION NO. (if
known, see 37 CFR 1.5)

09/937241

INTERNATIONAL APPLICATION NO.

INTERNATIONAL FILING DATE

PRIORITY DATE CLAIMED

PCT/GB00/01070

21 March 2000

23 March 1999

TITLE OF THE INVENTION

METHOD AND APPARATUS FOR THE DRYING OF NATURAL GAS

APPLICANT(S) FOR DO/EO/US

Finn Patrick NILSEN, Harald LINGA

Applicant hereby submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. ☒ This is the **FIRST** submission of items concerning a filing under 35 U.S.C. 371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. 371.
3. ☐ This express request to begin national examination procedures (35 U.S.C. 371 (f)) at any time rather than delay examination until the expiration of the applicable time limits set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(1).
4. ☒ A proper Demand for International Preliminary examination was made by the 19th month from the earliest claimed priority date.
5. ☒ A copy of the International Application as filed (35 U.S.C. 371(c)(2)).
 - a. ☐ is transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☒ has been transmitted by the International Bureau.
 - c. ☐ is not required, as the application was filed in the United States Receiving Office (RO/US).
6. ☒ A translation of the International Application into English (35 U.S.C. 371(c)(2).
7. ☒ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3)).
 - a. ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☐ have been transmitted by the International Bureau.
 - c. ☐ have not been made; however, the time limit for making such amendments has NOT expired.
 - d. ☒ have not been made.

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8. ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).
9. ☐ An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).
10. ☒ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).

Items 11. to 16. below concern document(s) or information included:

11. ☒ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
12. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
13. ☒ A FIRST preliminary amendment.
☐ A SECOND or SUBSEQUENT preliminary amendment.
14. ☒ A substitute specification.
15. ☐ A change of power of attorney and/or address letter.
16. ☒ Other items or information: International Search Report and Preliminary Examination Report, (Cited references are with the attached PTO 1449), Copy of PCT Request, Front Page of PCT Published Application, and Return Postcard

17. ☒ The following fees are submitted:

BASIC NATIONAL FEE (37 CFR 1.492 (a) (1)-(5))

Search Report has been prepared by the EPO or JPO.....\$860.00

International preliminary examination fee paid to USPTO
(37 CFR 1.482).....\$690.00

No international preliminary examination fee paid to USPTO
(37 CFR 1.482) but international search fee (37 CFR 1.445(a)(2))
paid to USPTO.....\$710.00

Neither international preliminary examination fee (37 CFR 1.482)
nor international search fee (37 CFR 1.445(a)(2)) paid to
USPTO.....\$1,000.00

International preliminary examination fee paid to USPTO
(37 CFR 1.482) and all claims satisfied provisions of
PCT Article 33(2)-(4).....\$100.00

ENTER APPROPRIATE BASIC FEE AMOUNT =

Surcharge of \$130.00 for furnishing the oath or declaration later
than ☐ 20 ☐ 30 months from the earliest claimed priority
date (37 CFR 1.492(e))

CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE		
Total claims	32 - 20 =	12	X \$18.00	\$216.00	
Independent claims	3 - 3 =	0	X \$80.00	\$0	
Multiple Dependent Claim(s) (If applicable)			X \$270.00	\$0	
TOTAL OF ABOVE CALCULATIONS =				\$1076.00	
Reduction of 1/2 for filing by small entity, if applicable. Verified Small Entity Statement must also be filed (Note 37 CFR 1.9, 1.27,				\$	

CALCULATIONS (PTO USE ONLY)

\$860.00

\$0.00

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1.28)		
SUBTOTAL =	\$1076.00	
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)).	\$0.00	
	+	
TOTAL NATIONAL FEE =	\$1076.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property	\$	
	+	
TOTAL FEES ENCLOSED =	\$1076.00	
	Amount to be:	\$
	refunded	
	charged	\$

a. ☒ A check in the amount of \$1076.00 to cover the above fees is enclosed

b. ☐ Please charge my Deposit Account No. **16-0631** in the amount of \$ _____ to cover the above fees. A duplicate copy of this sheet is enclosed.

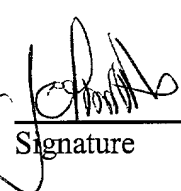
c. ☒ The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. 16-0631. A duplicate copy of this sheet is enclosed.

NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.

SEND ALL CORRESPONDENCE TO:

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Signature

John F. Thuent

Name

29,595

Registration Number

September 21, 2001

Date

09/937241

PATENT APPLICATION

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re the application of:

Attorney Docket No.: 1101.104US01

Nilsen et al.

Application No.: Based on PCT Application No. PCT/US00/01070

Filed: September 21, 2001

For: METHOD AND APPARATUS FOR THE DRYING OF NATURAL GAS

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents
Washington, D.C. 20231

Sir:

Prior to examination, please amend the above-identified application as follows:

In the Specification

Please substitute the following specification. No new matter has been added. The specification has been amended to conform to U.S. practice.

Method and Apparatus for the Drying of Natural Gas

Technical Field

The present invention is concerned with a method and apparatus for the removal of water from natural gas.

Background of the Invention

Natural gas as extracted from reservoirs contains water vapour. The concentration of the water vapour depends on the temperature and pressure of the gas at the extraction point. During the processing of the gas, particularly if it is treated to remove acid gas components such as carbon dioxide, CO₂, and hydrogen sulphide, H₂S, it may come into contact with aqueous solvents. This means that the gas may pick up further water vapour. When the gas is contacted with an aqueous solvent, it will become saturated with water vapour at the prevailing temperature and pressure. Before the gas is exported from the production facility the water vapour concentration in the gas must be reduced to very low levels. A typical specification may be 0.2 parts per million by volume (ppm v/v) of water in the gas. This is well below the concentrations which will normally be in the gas as extracted and well below the value after processing to remove CO₂ and/or H₂S. The gas, therefore has to be dried before it can be compressed for export.

Currently, the processes are generally used to dry a gas. These are based on absorption or adsorption respectively. In the adsorption, the gas is contacted with a porous solid material. The water vapour adsorbs onto the surface of the solid. The adsorbent is usually a silicious material, typically a mixture of aluminium and silica oxides known as molecular sieves. In absorption the gas is contacted with a chemical reagent which removes the water. The present application is concerned with absorption drying-dehydration processes.

In conventional drying processes alcohols, usually the glycols, monoethylene glycol, MEG, or triethylene glycol, TEG, are contacted with gas in a countercurrent tower. The gas is normally saturated with water vapour at the inlet conditions, temperature and pressure. The

saturation concentration increases with increasing temperature and decreasing pressure. In a typical set of conditions, 80 °C and 70B (7 x 10⁶ Pa) pressure, the saturation concentration is 8 x 10⁻³ kg/mm³ of gas. The concentration of water in the outlet gas will vary slightly with conditions on pipe line specifications but is typically of the order of 6.4 x 10⁻⁵ kg/mm³ of gas. This corresponds to a water dew point at 70Bg of -7 °C, well below the hydrate formation point.

In order to assess the absorption duty between these low concentrations, the thermodynamic equilibrium data - concentration of water in the gas, y^* , and concentration of water in the liquid phase, x - is required. Note:-

$$y^*_p = f(x)_p \quad (1)$$

i.e., the function f is dependent on the pressure.

The relevant data shows that the separation can be achieved in one theoretical stage, i.e. if equilibrium were achieved in the contacting (mixing) process, then one contact between the gas and liquid should give the required duty of water removal from the gas.

However, in conventional countercurrent tower units, 4 actual stages are normally specified. Stage efficiencies greater than 50% are simply not achieved.

Summary of the Invention

It is therefore an object of the invention to provide a method and apparatus which enables water vapour to be removed from a natural gas with greater efficiency.

According to the invention, there is provided a method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

While the invention has been described in relation to natural gas, it is equally applicable to other gases with a water content which it is desirable to reduce.

The invention also extends to the apparatus for carrying out this method.

The turbulent mixing is very intense and results in extremely efficient gas liquid contact. The mixing regime is preferably turbulent shear layer mixing. The liquid entrained in the gas may be in the form of droplets for gas continuous fluid phase distribution. The efficient mixing means that absorption can take place very rapidly and in a relatively small total volume of absorbent compared to that required in conventional absorption columns. The mixing system used is simple and inexpensive compared to prior art systems, leading to reduced costs. Finally, an efficiency of approaching 100% for the removal of water can be achieved for certain applications.

The advantages of such a mixer in relation to conventional countercurrent dehydration towers are a reduction in the size and weight of the equipment.

Preferably, the method is carried out as a continuous process with the natural gas and liquid flowing co-currently. The co-current flow reduces the problems associated with foaming and flooding, since absorption can continue downstream of the contactor.

One suitable contactor is a mixer supplied by Framo Engineering A/S and is described in EP-B-379319.

Preferably, the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet. In one possible regime, the natural gas is supplied to the tube, optionally directly, and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed. In another regime, the natural gas is supplied to the vessel and the liquid is supplied to the tube, optionally directly, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed. In a third regime, the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above the level of the outlet, whereby the natural gas is forced out through the outlet via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

Preferably, the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the homogeneous mixtures optionally being cooled prior to separation into a gas phase and a liquid phase. Preferably, the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone. Preferably, the absorbent in the liquid phase is subjected to a regeneration treatment to remove the absorbed water. Preferably, the regenerated absorbent-containing liquid phase is recycled to the contactor. Preferably, the regeneration is carried out by heating and/or by flashing off the water. Where the absorbent is a glycol, regeneration may be carried out by heating

the solution to about 200 °C and passing the vapours to a fractionating tower. Preferably, the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.

Partial recovery of the glycol may be attained by flashing off the water vapour by reducing the applied pressure on the liquid after gas dehydration. Where this is used then a similar turbulent mixer may be considered for this duty. This flashing operation will only give a partial glycol regeneration. In order to get to the very low levels of water content of the glycol solutions necessary for gas dehydration, heating of the solvent phase is required.

According to a more specific aspect of the invention, there is provided a method for removing water from a natural gas which comprises: supplying the natural gas to a turbulent contactor; supplying a liquid including an absorbent for the water to the contactor; subjecting the natural gas and the liquid to turbulent mixing in the contactor to form a homogeneous mixture; allowing the water to be absorbed by the absorbent; separating the homogeneous mixture into a gas phase and a liquid phase in a hydrocyclone (or any other gas/liquid separator); removing the gas phase; subjecting the solvent in the liquid phase to a regeneration treatment to remove the absorbed water; and recycling the regenerated absorbent-containing liquid phase to the contactor.

A portion of the solvent, after extraction may be recycled directed to the contactor.

Preferably, the absorbent includes a glycol or another water-miscible liquid. Preferably, the glycol is ethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these. The chosen absorbent could also be immiscible with water and in this case, a facility for separating the water from the absorbent would need to be introduced downstream of the gas/liquid separator.

Diethylene glycol (DEG) and monoethylene glycol (MEG) are typical solvents for dehydration. Triethylene glycol (TEG) is currently the most popular solvent since it has a higher

degradation temperature and can be regenerated to a higher lean concentration with no modification to a standard boiler. There has recently been a trend towards the reduction in BTEX (benzene, toluene, ethylbenzene, xylene) emissions which has in some cases favoured the use of MEG due to the much lower solubility of BTEX in this solvent. The penalty, however, is much higher glycol losses. The present invention envisages the use of any dehydration agent. However, the short residence time in the preferred contactor system (as compared with a counter-current absorption column) will necessarily result in less co-absorption of BTEX components in a given glycol system.

Preferably the natural gas and liquid are subjected to two or more mixing steps. Additional mixing steps may be carried out before and/or after the turbulent mixing step. One or more (or indeed all) of the additional mixing steps may themselves be turbulent mixing steps. They might be carried out using a similar turbulent contactor, or some other turbulent contactor, such as an ejector, a jet pump, or a mixer as described in WO 95/02448. Preferably, there are two or more turbulent mixing steps.

When second turbulent mixing is adopted, it is preferably conducted in a turbulent contactor comprising at least one fluid inlet, an outlet leading to a venturi passage, and a tube extending from the outlet back into the contactor. Preferably, the second contactor has a gas inlet and a liquid inlet. The tube may or may not be perforated, and the gap between the tube and the outlet may be varied. Preferably, the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor. The second turbulent contactor may also have a separate liquid inlet for the addition of fresh absorbent.

The invention also extends to apparatus for carrying out such a method, comprising: a turbulent contactor having a liquid inlet, a gas inlet and a fluid outlet; an optional cooler for the fluid

stream from the fluid outlet; a hydrocyclone arranged to separate the fluid stream into a gas phase and a liquid stream; a regenerator arranged to treat the separated liquid stream; and a recycle line arranged to convey the regenerated liquid stream to the contactor.

The apparatus may include a recycle line for the liquid stream from the separator to the contactor, by-passing the regenerator. There may also be a further separator, for example, in the form of a flash tank, in the recycle line to allow absorbed water to be released from the liquid.

The apparatus may include a pump arranged to supply liquid to the liquid inlet of the contactor. Preferably, the regenerator is a heater and/or a flash tank.

The invention may be considered to extend to the use of a turbulent contactor to remove water from natural gas by forming a homogeneous mixture of the gas mixture with an absorbent for the water in the contactor, allowing the water to be absorbed by the absorbent, and subsequently separating a gas phase and a liquid phase, the liquid phase thereby containing the water.

Brief Description of the Drawings

The invention may be put into practice in various ways and some embodiments will be described by way of example to illustrate the invention with reference to the accompanying drawings, in which:

Figure 1 is a flow diagram of a process in accordance with the invention;

Figure 2 is a view of the contacting section of the apparatus; and

Figure 3 is a view of the glycol separation and regeneration sections.

Detailed Description of the Drawings

Figure 1 shows a process for removing water from a gas stream, in accordance with the invention. The process comprises a turbulent contactor stage 11, a gas liquid separator 12, a depressurizer 13 and a glycol regeneration stage 14. Water-bearing natural gas is fed to the contactor at 15 and a triethylene glycol (TEG) absorbent at 16. In the contactor 11, the TEG absorbs the water from the natural gas and a homogeneous gas/liquid mixture leaves the contactor at 17.

The mixture is conveyed via line 18 to the separator 12 where the gas and liquid phases are separated. A water-free gas phase leaves the separator 12 at 19 and a liquid phase, comprising TEG and absorbed water is removed at 21.

This liquid phase is conveyed via a line 22 to a depressuriser 13 where water vapour is flashed off and removed via a water vapour outlet 23. The TEG with the remaining water is conveyed via a line 24 to the glycol regeneration stage 14, from which glycol is removed via a glycol outlet 25 and water is removed via a water outlet 26. The regenerated glycol can be recycled to the glycol inlet 16 to the contactor stage 11.

The contactor stage 11 is shown in more detail in Figure 2. This stage 11 comprises two stages. The turbulent contactor 100 forming the first stage comprises a vessel 101 having the natural gas inlet 15, the glycol inlet 16 and an outlet 104 leading to a venturi passage 105. There is a tube 106 (which may or may not be perforated) extending from the outlet 104 back into the vessel 101.

The glycol and the natural gas are supplied to the vessel 101, the glycol being supplied to a level above the level of the outlet 104, whereby the gas is forced out through the outlet 104 via the tube 106, thereby drawing the glycol into the venturi so that the two phases are mixed.

The homogeneous gas/liquid mixture from the first turbulent contactor 100 is conveyed to a second turbulent contactor 110. Thus, the mixture enters an annular flow generator 150 from a spool piece 151, or directly from the diffuser of the venturi 105. As the gas/liquid mixture flows through the expanding outlet part of the annular flow generator 150, a liquid film establishes at the wall to form an annular gas/liquid flow essentially with the gas in the pipe core and the liquid at the pipe wall. The liquid film will be maintained in the annulus between inner and outer pipes 152 and 153 respectively.

The conditions at the outlet 154 of the inner pipe 152 are similar to the conditions at the outlet 104 of the first turbulent contactor. It is clear that, in principle, any number of stages can be added to the system, although considerations such as pressure drop should be taken into account.

As shown in Figure 2, the mixture leaving the second contactor 110 at the outlet 17 is conveyed to a hydrocyclone gas liquid separator 12 via a tangential inlet 31 (see Fig. 3). The two phases present are separated in the normal way. The gas phase, comprising dehydrated natural gas, passes upwards via a centre tube 32 and two demister stages 33,34, and leaves via the gas outlet 19. The liquid phase, comprising glycol and absorbed water, passes downwards via a conical collector 35 and leaves via the liquid outlet 21. Accumulated liquid can be drained from tubes at 37 at the level of the support ring for the centre tube 32.

The liquid is conveyed to a depressuriser 13, where some of the absorbed water is flashed off and leaves via the water vapour outlet 23. The glycol and any remaining absorbed water is

pumped to the glycol regenerator 14 via the line 24. Here, the remaining absorbed water is separated from the glycol. The water is removed via the outlet 25 and dehydrated glycol is removed via the glycol outlet 26. This regenerated glycol is then recycled to the glycol inlet 16 to the contactor stage 11, via a recycle line 36.

In the Claims

Please cancel claims 1-32 without prejudice or disclaimer.

Please add new claims 33-64 as follows:

33. A method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

34. A method as claimed Claim 33, in which the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet.

35. A method as claimed in Claim 34, in which the natural gas is supplied to the tube and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed.

36. A method as claimed in Claim 34, in which the natural gas is supplied to the vessel and the liquid is supplied to the tube, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed.

37. A method as claimed in Claim 34, in which the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above the level of the outlet, whereby the natural gas is forced out through the outlet via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

38. A method as claimed in Claim 33, in which the method is carried out as a continuous process with the natural gas and liquid flowing co-currently.

39. A method as claimed in Claim 33, in which the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the homogeneous mixture optionally being cooled prior to separation into a gas phase and a liquid phase.

40. A method as claimed in Claim 39, in which the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone.

41. A method as claimed in Claim 33, in which the absorbent in the liquid phase is subjected to a regeneration treatment to remove the absorbed water.

42. A method as claimed in Claim 41, in which the regenerated absorbent-containing liquid phase is recycled to the contactor.
43. A method as claimed in Claim 42, in which the regeneration is carried out by heating and/or by flashing off the absorbed water.
44. A method as claimed in Claim 43, in which the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.
45. A method as claimed in Claim 33, in which the absorbent is miscible with water.
46. A method as claimed in Claim 33, in which the absorbent is immiscible with water.
47. A method as claimed in Claim 33, in which the absorbent includes a glycol.
48. A method as claimed in Claim 47, in which the absorbent is monoethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these.
49. A method as claimed in Claim 33, in which the natural gas and liquid are subjected to two or more mixing steps.

50. A method as claimed in Claim 49, in which an additional mixing step is carried out before the turbulent mixing step.

51. A method as claimed in Claim 49, in which an additional mixing step is carried out after the turbulent mixing step.

52. A method as claimed in Claim 50, in which one or more additional mixing steps are turbulent mixing steps.

53. A method as claimed in Claim 52, in which a second mixing step is carried out in a second contactor, located in a pipe extending from the venturi passage of the first contactor.

54. A method as claimed in Claim 53, in which the fluid mixture is separated into a gas phase and a liquid phase between the two contactors, the phase separation preferably occurring in an annular flow generator.

55. A method as claimed in Claim 53, in which fresh liquid solvent is added to the second contactor.

56. Apparatus for removing water from natural gas by bringing the natural gas into contact with a liquid including an absorbent for the water, comprising: a turbulent contactor in which the natural gas and liquid are subjected to turbulent mixing conditions thereby causing the water to be absorbed

by the absorbent; and a separator for separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the turbulent contactor comprises a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

57. Apparatus as claimed Claim 56, in which the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet.

58. Apparatus as claimed in Claim 56, in which the separator includes a hydrocyclone.

59. Apparatus as claimed in Claim 56, in which the separator includes an absorbent regenerator.

60. Apparatus as claimed in Claim 56, in which the contactor includes two or more contactor steps.

61. Apparatus as claimed in Claim 60, in which the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor.

62. The use of one or more turbulent contactor for absorbing water from a natural gas stream, in which the gas stream is brought into contact with a liquid including an absorbent for water, at least

one of the turbulent contactors comprising a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream.

63. A use as claimed in Claim 62, in which the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor.

64. A use as claimed in Claim 62, in which a gas phase and a liquid phase are separated after exit from a first turbulent contactor before entry into a second turbulent contactor, the phase separation preferably occurring in an annular flow generator.

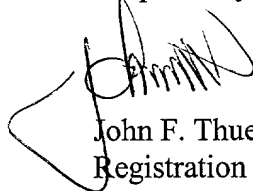
REMARKS

Claims 1-32 are pending. By this Amendment, claims 1-32 are canceled and new claims 33-64 are added. Claims 33-64 are not narrowed with respect to claims 1-32, but are submitted herewith solely for purpose of conforming the application to U.S. practice.

In view of the foregoing, it is submitted that this application is in condition for allowance. Favorable consideration and prompt allowance of the application are respectfully requested.

The Examiner is invited to telephone the undersigned if the Examiner believes it would be useful to advance prosecution.

Respectfully submitted,



John F. Thunte
Registration No. 29,595

Based on PCT Application No. PCT/US00/01070

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ATTACHMENT
REDLINED AMENDMENT

Specification As Amended

Please substitute the following specification:

Method and Apparatus for the Drying of Natural Gas

Technical Field

The present invention is concerned with a method and apparatus for the removal of water from natural gas.

Background of the Invention

Natural gas as extracted from reservoirs contains water vapour. The concentration of the water vapour depends on the temperature and pressure of the gas at the extraction point. During the processing of the gas, particularly if it is treated to remove acid gas components such as carbon dioxide, CO₂, and hydrogen sulphide, H₂S, it may come into contact with aqueous solvents. This means that the gas may pick up further water vapour. When the gas is contacted with an aqueous solvent, it will become saturated with water vapour at the prevailing temperature and pressure. Before the gas is exported from the production facility the water vapour concentration in the gas must be reduced to very low levels. A typical specification may be 0.2 parts per million by volume (ppm v/v) of water in the gas. This is well below the concentrations which will normally be in the gas as extracted and well below the value after processing to remove CO₂ and/or H₂S. The gas, therefore has to be dried before it can be compressed for export.

Currently, the processes are generally used to dry a gas. These are based on absorption or adsorption respectively. In the adsorption, the gas is contacted with a porous solid material. The water vapour adsorbs onto the surface of the solid. The adsorbent is usually a silicious material, typically a mixture of aluminium and silica oxides known as molecular sieves. In absorption the gas is contacted with a chemical reagent which removes the water. The present application is concerned with absorption drying-dehydration processes.

In conventional drying processes alcohols, usually the glycols, monoethylene glycol, MEG, or triethylene glycol, TEG, are contacted with gas in a countercurrent tower. The gas is normally saturated with water vapour at the inlet conditions, temperature and pressure. The saturation concentration increases with increasing temperature and decreasing pressure. In a typical set of conditions, 80 °C and 70B (7 x 10⁶ Pa) pressure, the saturation concentration is 8 x 10⁻³ kg/mm³cm of gas. The concentration of water in the outlet gas will vary slightly with conditions on pipe line specifications but is typically of the order of 6.4 x 10⁻⁵ kg/mm³cm of gas. This corresponds to a water dew point at 70Bg of -7 °C, well below the hydrate formation point.

In order to assess the absorption duty between these low concentrations, the thermodynamic equilibrium data - concentration of water in the gas, y^* , and concentration of water in the liquid phase, x - is required. Note:-

$$y^*_p = f(x)_p \quad (1)$$

i.e., the function f is dependent on the pressure.

The relevant data shows that the separation can be achieved in one theoretical stage, i.e. if equilibrium were achieved in the contacting (mixing) process, then one contact between the gas and liquid should give the required duty of water removal from the gas.

However, in conventional countercurrent tower units, 4 actual stages are normally specified. Stage efficiencies greater than 50% are simply not achieved.

Summary of the Invention

It is therefore an object of the invention to provide a method and apparatus which enables water vapour to be removed from a natural gas with greater efficiency.

According to the invention, there is provided a method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

While the invention has been described in relation to natural gas, it is equally applicable to other gases with a water content which it is desirable to reduce.

The invention also extends to the apparatus for carrying out this method.

The turbulent mixing is very intense and results in extremely efficient gas liquid contact. The mixing regime is preferably turbulent shear layer mixing. The liquid entrained in the gas may

be in the form of droplets for gas continuous fluid phase distribution. The efficient mixing means that absorption can take place very rapidly and in a relatively small total volume of absorbent compared to that required in conventional absorption columns. The mixing system used is simple and inexpensive compared to prior art systems, leading to reduced costs. Finally, an efficiency of approaching 100% for the removal of water can be achieved for certain applications.

The advantages of such a mixer in relation to conventional countercurrent dehydration towers are a reduction in the size and weight of the equipment.

Preferably, the method is carried out as a continuous process with the natural gas and liquid flowing co-currently. The co-current flow reduces the problems associated with foaming and flooding, since absorption can continue downstream of the contactor.

One suitable contactor is a mixer supplied by Framo Engineering A/S and is described in EP-B-379319.

Preferably, the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet. In one possible regime, the natural gas is supplied to the tube, optionally directly, and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed. In another regime, the natural gas is supplied to the vessel and the liquid is supplied to the tube, optionally directly, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed. In a third regime, the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above the level of the outlet, whereby the natural gas is forced out through the outlet via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

Preferably, the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the homogeneous mixtures optionally being cooled prior to separation into a gas phase and a liquid phase. Preferably, the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone. Preferably, the absorbent in the liquid phase is subjected to a regeneration treatment to remove the absorbed water. Preferably, the regenerated absorbent-containing liquid phase is recycled to the contactor. Preferably, the regeneration is carried out by heating and/or by flashing off the water. Where the absorbent is a glycol, regeneration may be carried out by heating the solution to about 200 °C and passing the vapours to a fractionating tower. Preferably, the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.

Partial recovery of the glycol may be attained by flashing off the water vapour by reducing the applied pressure on the liquid after gas dehydration. Where this is used then a similar turbulent mixer may be considered for this duty. This flashing operation will only give a partial glycol regeneration. In order to get to the very low levels of water content of the glycol solutions necessary for gas dehydration, heating of the solvent phase is required.

According to a more specific aspect of the invention, there is provided a method for removing water from a natural gas which comprises: supplying the natural gas to a turbulent contactor; supplying a liquid including an absorbent for the water to the contactor; subjecting the natural gas and the liquid to turbulent mixing in the contactor to form a homogeneous mixture; allowing the water to be absorbed by the absorbent; separating the homogeneous mixture into a gas phase and a liquid phase in a hydrocyclone (or any other gas/liquid separator); removing the gas phase; subjecting the solvent in the liquid phase to a regeneration treatment to remove the absorbed water; and recycling the regenerated absorbent-containing liquid phase to the contactor.

A portion of the solvent, after extraction may be recycled directed to the contactor.

Preferably, the absorbent includes a glycol or another water-miscible liquid. Preferably, the glycol is ethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these. The chosen absorbent could also be immiscible with water and in this case, a facility for separating the water from the absorbent would need to be introduced downstream of the gas/liquid separator.

Diethylene glycol (DEG) and monoethylene glycol (MEG) are typical solvents for dehydration. Triethylene glycol (TEG) is currently the most popular solvent since it has a higher degradation temperature and can be regenerated to a higher lean concentration with no modification to a standard boiler. There has recently been a trend towards the reduction in BTEX (benzene, toluene, ethylbenzene, xylene) emissions which has in some cases favoured the use of MEG due to the much lower solubility of BTEX in this solvent. The penalty, however, is much higher glycol losses. The present invention envisages the use of any dehydration agent. However, the short residence time in the preferred contactor system (as compared with a counter-current absorption column) will necessarily result in less co-absorption of BTEX components in a given glycol system.

Preferably the natural gas and liquid are subjected to two or more mixing steps. Additional mixing steps may be carried out before and/or after the turbulent mixing step. One or more (or indeed all) of the additional mixing steps may themselves be turbulent mixing steps. They might be carried out using a similar turbulent contactor, or some other turbulent contactor, such as an ejector, a jet pump, or a mixer as described in WO 95/02448. Preferably, there are two or more turbulent mixing steps.

When second turbulent mixing is adopted, it is preferably conducted in a turbulent contactor comprising at least one fluid inlet, an outlet leading to a venturi passage, and a tube extending from

the outlet back into the contactor. Preferably, the second contactor has a gas inlet and a liquid inlet. The tube may or may not be perforated, and the gap between the tube and the outlet may be varied. Preferably, the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor. The second turbulent contactor may also have a separate liquid inlet for the addition of fresh absorbent.

The invention also extends to apparatus for carrying out such a method, comprising: a turbulent contactor having a liquid inlet, a gas inlet and a fluid outlet; an optional cooler for the fluid stream from the fluid outlet; a hydrocyclone arranged to separate the fluid stream into a gas phase and a liquid stream; a regenerator arranged to treat the separated liquid stream; and a recycle line arranged to convey the regenerated liquid stream to the contactor.

The apparatus may include a recycle line for the liquid stream from the separator to the contactor, by-passing the regenerator. There may also be a further separator, for example, in the form of a flash tank, in the recycle line to allow absorbed water to be released from the liquid.

The apparatus may include a pump arranged to supply liquid to the liquid inlet of the contactor. Preferably, the regenerator is a heater and/or a flash tank.

The invention may be considered to extend to the use of a turbulent contactor to remove water from natural gas by forming a homogeneous mixture of the gas mixture with an absorbent for the water in the contactor, allowing the water to be absorbed by the absorbent, and subsequently separating a gas phase and a liquid phase, the liquid phase thereby containing the water.

Brief Description of the Drawings

The invention may be put into practice in various ways and some embodiments will be described by way of example to illustrate the invention with reference to the accompanying drawings, in which:

Figure 1 is a flow diagram of a process in accordance with the invention;

Figure 2 is a view of the contacting section of the apparatus; and

Figure 3 is a view of the glycol separation and regeneration sections.

Detailed Description of the Drawings

Figure 1 shows a process for removing water from a gas stream, in accordance with the invention. The process comprises a turbulent contactor stage 11, a gas liquid separator 12, a depressurizer 13 and a glycol regeneration stage 14. Water-bearing natural gas is fed to the contactor at 15 and a triethylene glycol (TEG) absorbent at 16. In the contactor 11, the TEG absorbs the water from the natural gas and a homogeneous gas/liquid mixture leaves the contactor at 17.

The mixture is conveyed via line 18 to the separator 12 where the gas and liquid phases are separated. A water-free gas phase leaves the separator 12 at 19 and a liquid phase, comprising TEG and absorbed water is removed at 21.

This liquid phase is conveyed via a line 22 to a depressuriser 13 where water vapour is flashed off and removed via a water vapour outlet 23. The TEG with the remaining water is conveyed via a line 24 to the glycol regeneration stage 14, from which glycol is removed via a

glycol outlet 25 and water is removed via a water outlet 26. The regenerated glycol can be recycled to the glycol inlet 16 to the contactor stage 11.

The contactor stage 11 is shown in more detail in Figure 2. This stage 11 comprises two stages. The turbulent contactor 100 forming the first stage comprises a vessel 101 having the natural gas inlet 15, the glycol inlet 16 and an outlet 104 leading to a venturi passage 105. There is a tube 106 (which may or may not be perforated) extending from the outlet 104 back into the vessel 101.

The glycol and the natural gas are supplied to the vessel 101, the glycol being supplied to a level above the level of the outlet 104, whereby the gas is forced out through the outlet 104 via the tube 106, thereby drawing the glycol into the venturi so that the two phases are mixed.

The homogeneous gas/liquid mixture from the first turbulent contactor 100 is conveyed to a second turbulent contactor 110. Thus, the mixture enters an annular flow generator 150 from a spool piece 151, or directly from the diffuser of the venturi 105. As the gas/liquid mixture flows through the expanding outlet part of the annular flow generator 150, a liquid film establishes at the wall to form an annular gas/liquid flow essentially with the gas in the pipe core and the liquid at the pipe wall. The liquid film will be maintained in the annulus between inner and outer pipes 152 and 153 respectively.

The conditions at the outlet 154 of the inner pipe 152 are similar to the conditions at the outlet 104 of the first turbulent contactor. It is clear that, in principle, any number of stages can be added to the system, although considerations such as pressure drop should be taken into account.

As shown in Figure 2, the mixture leaving the second contactor 110 at the outlet 17 is conveyed to a hydrocyclone gas liquid separator 12 via a tangential inlet 31 (see Fig. 3). The two

phases present are separated in the normal way. The gas phase, comprising dehydrated natural gas, passes upwards via a centre tube 32 and two demistor stages 33,34, and leaves via the gas outlet 19. The liquid phase, comprising glycol and absorbed water, passes downwards via a conical collector 35 and leaves via the liquid outlet 21. Accumulated liquid can be drained from tubes at 37 at the level of the support ring for the centre tube 32.

The liquid is conveyed to a depressuriser 13, where some of the absorbed water is flashed off and leaves via the water vapour outlet 23. The glycol and any remaining absorbed water is pumped to the glycol regenerator 14 via the line 24. Here, the remaining absorbed water is separated from the glycol. The water is removed via the outlet 25 and dehydrated glycol is removed via the glycol outlet 26. This regenerated glycol is then recycled to the glycol inlet 16 to the contactor stage 11, via a recycle line 36.

Claims As Amended

Please cancel claims 1-32 without prejudice or disclaimer.

Please add new claims 33-64 as follows:

Please substitute the following amended claims for those currently pending:

33. A method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas

inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

34. A method as claimed Claim 33, in which the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet.

35. A method as claimed in Claim 34, in which the natural gas is supplied to the tube and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed.

36. A method as claimed in Claim 34, in which the natural gas is supplied to the vessel and the liquid is supplied to the tube, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed.

37. A method as claimed in Claim 34, in which the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above the level of the outlet, whereby the natural gas is forced out through the outlet via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

38. A method as claimed in Claim 33, in which the method is carried out as a continuous process with the natural gas and liquid flowing co-currently.

39. A method as claimed in Claim 33, in which the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the homogeneous mixture optionally being cooled prior to separation into a gas phase and a liquid phase.

40. A method as claimed in Claim 39, in which the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone.

41. A method as claimed in Claim 33, in which the absorbent in the liquid phase is subjected to a regeneration treatment to remove the absorbed water.

42. A method as claimed in Claim 41, in which the regenerated absorbent-containing liquid phase is recycled to the contactor.

43. A method as claimed in Claim 42, in which the regeneration is carried out by heating and/or by flashing off the absorbed water.

44. A method as claimed in Claim 43, in which the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.

45. A method as claimed in Claim 33, in which the absorbent is miscible with water.

46. A method as claimed in Claim 33, in which the absorbent is immiscible with water.

47. A method as claimed in Claim 33, in which the absorbent includes a glycol.
48. A method as claimed in Claim 47, in which the absorbent is monoethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these.
49. A method as claimed in Claim 33, in which the natural gas and liquid are subjected to two or more mixing steps.
50. A method as claimed in Claim 49, in which an additional mixing step is carried out before the turbulent mixing step.
51. A method as claimed in Claim 49, in which an additional mixing step is carried out after the turbulent mixing step.
52. A method as claimed in Claim 50, in which one or more additional mixing steps are turbulent mixing steps.
53. A method as claimed in Claim 52, in which a second mixing step is carried out in a second contactor, located in a pipe extending from the venturi passage of the first contactor.

54. A method as claimed in Claim 53, in which the fluid mixture is separated into a gas phase and a liquid phase between the two contactors, the phase separation preferably occurring in an annular flow generator.

55. A method as claimed in Claim 53, in which fresh liquid solvent is added to the second contactor.

56. Apparatus for removing water from natural gas by bringing the natural gas into contact with a liquid including an absorbent for the water, comprising: a turbulent contactor in which the natural gas and liquid are subjected to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and a separator for separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the turbulent contactor comprises a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

57. Apparatus as claimed Claim 56, in which the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet.

58. Apparatus as claimed in Claim 56, in which the separator includes a hydrocyclone.

59. Apparatus as claimed in Claim 56, in which the separator includes an absorbent regenerator.

60. Apparatus as claimed in Claim 56, in which the contactor includes two or more contactor steps.

61. Apparatus as claimed in Claim 60, in which the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor.

62. The use of one or more turbulent contactor for absorbing water from a natural gas stream, in which the gas stream is brought into contact with a liquid including an absorbent for water, at least one of the turbulent contactors comprising a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream.

63. A use as claimed in Claim 62, in which the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor.

64. A use as claimed in Claim 62, in which a gas phase and a liquid phase are separated after exit from a first turbulent contactor before entry into a second turbulent contactor, the phase separation preferably occurring in an annular flow generator.

SUBSTITUTE SPECIFICATION

09/937241

Attorney Docket No. 1101.104US01

Method and Apparatus for the Drying of Natural GasTechnical Field

5 The present invention is concerned with a method and apparatus for the removal of water from natural gas.

Background of the Invention

10 Natural gas as extracted from reservoirs contains water vapour. The concentration of the water vapour depends on the temperature and pressure of the gas at the extraction point. During the processing of the gas, particularly if it is treated to remove acid gas components such as carbon dioxide, CO₂, and hydrogen sulphide, H₂S, it may come into contact with aqueous solvents. This means that the gas may pick up further water vapour. When the gas is contacted with an aqueous solvent, it will become saturated with water vapour at the prevailing temperature and pressure. Before the gas is exported from the production facility the water vapour concentration in the gas must be reduced to very low levels. A typical
15 specification may be 0.2 parts per million by volume (ppm v/v) of water in the gas. This is well below the concentrations which will normally be in the gas as extracted and well below the value after processing to remove CO₂ and/or H₂S. The gas, therefore has to be dried before it can be compressed for export.

20 Currently, the processes are generally used to dry a gas. These are based on absorption or adsorption respectively. In the adsorption, the gas is contacted with a porous solid material. The water vapour adsorbs onto the surface of the solid. The adsorbent is usually a silicious material, typically a mixture of aluminium and silica oxides known as molecular sieves. In absorption the gas is contacted with a chemical reagent which removes

the water. The present application is concerned with absorption drying-dehydration processes.

In conventional drying processes alcohols, usually the glycols, monoethylene glycol, MEG, or triethylene glycol, TEG, are contacted with gas in a countercurrent tower. The gas is normally saturated with water vapour at the inlet conditions, temperature and pressure. The saturation concentration increases with increasing temperature and decreasing pressure. In a typical set of conditions, 80 °C and 70B (7 x 10⁶ Pa) pressure, the saturation concentration is 8 x 10⁻³ kg/mm³ of gas. The concentration of water in the outlet gas will vary slightly with conditions on pipe line specifications but is typically of the order of 6.4 x 10⁻⁵ kg/mm³ of gas. This corresponds to a water low point at 70Bg of -7 °C, well below the hydrate formation point.

In order to assess the absorption duty between these low concentrations, the thermodynamic equilibrium data - concentration of water in the gas, y^* , and concentration of water in the liquid phase, x - is required. Note:-

$$y_p^* = f(x)_p \quad (1)$$

i.e., the function f is dependent on the pressure.

The relevant data shows that the separation can be achieved in one theoretical stage, i.e. if equilibrium were achieved in the contacting (mixing) process, then one contact between the gas and liquid should give the required duty of water removal from the gas.

However, in conventional countercurrent tower units, 4 actual stages are normally specified. Stage efficiencies greater than 50% are simply not achieved.

Summary of the Invention

It is therefore an object of the invention to provide a method and apparatus which enables water vapour to be removed from a natural gas with greater efficiency.

According to the invention, there is provided a method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

While the invention has been described in relation to natural gas, it is equally applicable to other gases with a water content which it is desirable to reduce.

The invention also extends to the apparatus for carrying out this method.

The turbulent mixing is very intense and results in extremely efficient gas liquid contact. The mixing regime is preferably turbulent shear layer mixing. The liquid entrained in the gas may be in the form of droplets for gas continuous fluid phase distribution. The efficient mixing means that absorption can take place very rapidly and in a relatively small total volume of absorbent compared to that required in conventional absorption columns. The mixing system used is simple and inexpensive compared to prior art systems, leading to reduced costs. Finally, an efficiency of approaching 100% for the removal of water can be achieved for certain applications.

The advantages of such a mixer in relation to conventional countercurrent dehydration towers are a reduction in the size and weight of the equipment.

Preferably, the method is carried out as a continuous process with the natural gas and liquid flowing co-currently. The co-current flow reduces the problems associated with foaming and flooding, since absorption can continue downstream of the contactor.

One suitable contactor is a mixer supplied by Framo Engineering A/S and is described in EP-B-379319.

Preferably, the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet. In one possible regime, the natural gas is supplied to the tube, optionally directly, and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed. In another regime, the natural gas is supplied to the vessel and the liquid is supplied to the tube, optionally directly, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed. In a third regime, the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above the level of the outlet, whereby the natural gas is forced out through the outlet via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

Preferably, the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the homogeneous mixtures optionally being cooled prior to separation into a gas phase and a liquid phase. Preferably, the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone. Preferably, the absorbent in the liquid phase is subjected to a regeneration treatment to remove the absorbed water. Preferably, the regenerated absorbent-containing liquid phase is recycled to the contactor. Preferably, the regeneration is carried out by heating and/or by flashing off the water. Where the absorbent is a glycol, regeneration may be carried out by heating the solution to about 200 °C and passing the vapours to a fractionating tower. Preferably, the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.

Partial recovery of the glycol may be attained by flashing off the water vapour by reducing the applied pressure on the liquid after gas dehydration. Where this is used then a similar turbulent mixer may be considered for this duty. This flashing operation will only give a partial glycol regeneration. In order to get to the very low levels of water content of the glycol solutions necessary for gas dehydration, heating of the solvent phase is required.

According to a more specific aspect of the invention, there is provided a method for removing water from a natural gas which comprises: supplying the natural gas to a turbulent contactor; supplying a liquid including an absorbent for the water to the contactor; subjecting the natural gas and the liquid to turbulent mixing in the contactor to form a homogeneous mixture; allowing the water to be absorbed by the absorbent; separating the homogeneous mixture into a gas phase and a liquid phase in a hydrocyclone (or any other gas/liquid separator); removing the gas phase; subjecting the solvent in the liquid phase to a regeneration treatment to remove the absorbed water; and recycling the regenerated absorbent-containing liquid phase to the contactor.

A portion of the solvent, after extraction may be recycled directed to the contactor.

Preferably, the absorbent includes a glycol or another water-miscible liquid. Preferably, the glycol is ethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these. The chosen absorbent could also be immiscible with water and in this case, a facility for separating the water from the absorbent would need to be introduced downstream of the gas/liquid separator.

Diethylene glycol (DEG) and monoethylene glycol (MEG) are typical solvents for dehydration. Triethylene glycol (TEG) is currently the most popular solvent since it has a higher degradation temperature and can be regenerated to a higher lean concentration with no modification to a standard boiler. There has recently been a trend towards the reduction in

BTEX (benzene, toluene, ethylbenzene, xylene) emissions which has in some cases favoured the use of MEG due to the much lower solubility of BTEX in this solvent. The penalty, however, is much higher glycol losses. The present invention envisages the use of any dehydration agent. However, the short residence time in the preferred contactor system (as compared with a counter-current absorption column) will necessarily result in less co-absorption of BTEX components in a given glycol system.

Preferably the natural gas and liquid are subjected to two or more mixing steps. Additional mixing steps may be carried out before and/or after the turbulent mixing step. One or more (or indeed all) of the additional mixing steps may themselves be turbulent mixing steps. They might be carried out using a similar turbulent contactor, or some other turbulent contactor, such as an ejector, a jet pump, or a mixer as described in WO 95/02448. Preferably, there are two or more turbulent mixing steps.

When second turbulent mixing is adopted, it is preferably conducted in a turbulent contactor comprising at least one fluid inlet, an outlet leading to a venturi passage, and a tube extending from the outlet back into the contactor. Preferably, the second contactor has a gas inlet and a liquid inlet. The tube may or may not be perforated, and the gap between the tube and the outlet may be varied. Preferably, the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor. The second turbulent contactor may also have a separate liquid inlet for the addition of fresh absorbent.

The invention also extends to apparatus for carrying out such a method, comprising: a turbulent contactor having a liquid inlet, a gas inlet and a fluid outlet; an optional cooler for the fluid stream from the fluid outlet; a hydrocyclone arranged to separate the fluid stream into a gas phase and a liquid stream; a regenerator arranged to treat the separated liquid stream; and a recycle line arranged to convey the regenerated liquid stream to the contactor.

The apparatus may include a recycle line for the liquid stream from the separator to the contactor, by-passing the regenerator. There may also be a further separator, for example, in the form of a flash tank, in the recycle line to allow absorbed water to be released from the liquid.

The apparatus may include a pump arranged to supply liquid to the liquid inlet of the contactor. Preferably, the regenerator is a heater and/or a flash tank.

The invention may be considered to extend to the use of a turbulent contactor to remove water from natural gas by forming a homogeneous mixture of the gas mixture with an absorbent for the water in the contactor, allowing the water to be absorbed by the absorbent, and subsequently separating a gas phase and a liquid phase, the liquid phase thereby containing the water.

Brief Description of the Drawings

The invention may be put into practice in various ways and some embodiments will be described by way of example to illustrate the invention with reference to the accompanying drawings, in which:

Figure 1 is a flow diagram of a process in accordance with the invention;

Figure 2 is a view of the contacting section of the apparatus; and

Figure 3 is a view of the glycol separation and regeneration sections.

Detailed Description of the Drawings

Figure 1 shows a process for removing water from a gas stream, in accordance with the invention. The process comprises a turbulent contactor stage 11, a gas liquid separator 12, a depressurizer 13 and a glycol regeneration stage 14. Water-bearing natural gas is fed to the contactor at 15 and a triethylene glycol (TEG) absorbent at 16. In the contactor 11, the TEG

absorbs the water from the natural gas and a homogeneous gas/liquid mixture leaves the contactor at 17.

The mixture is conveyed via line 18 to the separator 12 where the gas and liquid phases are separated. A water-free gas phase leaves the separator 12 at 19 and a liquid phase, comprising TEG and absorbed water is removed at 21.

This liquid phase is conveyed via a line 22 to a depressuriser 13 where water vapour is flashed off and removed via a water vapour outlet 23. The TEG with the remaining water is conveyed via a line 24 to the glycol regeneration stage 14, from which glycol is removed via a glycol outlet 25 and water is removed via a water outlet 26. The regenerated glycol can be recycled to the glycol inlet 16 to the contactor stage 11.

The contactor stage 11 is shown in more detail in Figure 2. This stage 11 comprises two stages. The turbulent contactor 100 forming the first stage comprises a vessel 101 having the natural gas inlet 15, the glycol inlet 16 and an outlet 104 leading to a venturi passage 105. There is a tube 106 (which may or may not be perforated) extending from the outlet 104 back into the vessel 101.

The glycol and the natural gas are supplied to the vessel 101, the glycol being supplied to a level above the level of the outlet 104, whereby the gas is forced out through the outlet 104 via the tube 106, thereby drawing the glycol into the venturi so that the two phases are mixed.

The homogeneous gas/liquid mixture from the first turbulent contactor 100 is conveyed to a second turbulent contactor 110. Thus, the mixture enters an annular flow generator 150 from a spool piece 151, or directly from the diffuser of the venturi 105. As the gas/liquid mixture flows through the expanding outlet part of the annular flow generator 150, a liquid film establishes at the wall to form an annular gas/liquid flow essentially with the gas in the pipe core

and the liquid at the pipe wall. The liquid film will be maintained in the annulus between inner and outer pipes 152 and 153 respectively.

The conditions at the outlet 154 of the inner pipe 152 are similar to the conditions at the outlet 104 of the first turbulent contactor. It is clear that, in principle, any number of stages can be added to the system, although considerations such as pressure drop should be taken into account.

As shown in Figure 2, the mixture leaving the second contactor 110 at the outlet 17 is conveyed to a hydrocyclone gas liquid separator 12 via a tangential inlet 31 (see Fig. 3). The two phases present are separated in the normal way. The gas phase, comprising dehydrated natural gas, passes upwards via a centre tube 32 and two demister stages 33,34, and leaves via the gas outlet 19. The liquid phase, comprising glycol and absorbed water, passes downwards via a conical collector 35 and leaves via the liquid outlet 21. Accumulated liquid can be drained from tubes at 37 at the level of the support ring for the centre tube 32.

The liquid is conveyed to a depressuriser 13, where some of the absorbed water is flashed off and leaves via the water vapour outlet 23. The glycol and any remaining absorbed water is pumped to the glycol regenerator 14 via the line 24. Here, the remaining absorbed water is separated from the glycol. The water is removed via the outlet 25 and dehydrated glycol is removed via the glycol outlet 26. This regenerated glycol is then recycled to the glycol inlet 16 to the contactor stage 11, via a recycle line 36.

09/937241

3/PATS

Method and Apparatus for the Drying of Natural Gas

The present invention is concerned with a method and apparatus for the removal of water from natural gas.

5 Natural gas as extracted from reservoirs contains water vapour. The concentration of the water vapour depends on the temperature and pressure of the gas at the extraction point. During the processing of the gas, particularly if it is treated to remove acid gas
10 components such as carbon dioxide, CO_2 , and hydrogen sulphide, H_2S , it may come into contact with aqueous solvents. This means that the gas may pick up further water vapour. When the gas is contacted with an aqueous solvent, it will become saturated with water vapour at the
15 prevailing temperature and pressure. Before the gas is exported from the production facility the water vapour concentration in the gas must be reduced to very low levels. A typical specification may be 0.2 parts per million by volume (ppm v/v) of water in the gas. This is
20 well below the concentrations which will normally be in the gas as extracted and well below the value after processing to remove CO_2 and/or H_2S . The gas, therefore has to be dried before it can be compressed for export.

Currently, the processes are generally used to dry a
25 gas. These are based on absorption or adsorption respectively. In the adsorption, the gas is contacted with a porous solid material. The water vapour adsorbs onto the surface of the solid. The adsorbent is usually a silicious material, typically a mixture of aluminium and
30 silica oxides known as molecular sieves. In absorption the gas is contacted with a chemical reagent which removes the water. The present application is concerned with absorption drying-dehydration processes.

In conventional drying processes alcohols, usually

the glycols, monoethylene glycol, MEG, or triethylene glycol, TEG, are contacted with gas in a countercurrent tower. The gas is normally saturated with water vapour at the inlet conditions, temperature and pressure. The
5 saturation concentration increases with increasing temperature and decreasing pressure. In a typical set of conditions, 80 °C and 70B (7 x 10⁶ Pa) pressure, the saturation concentration is 8 x 10⁻³ kg/mmscm of gas. The
10 concentration of water in the outlet gas will vary slightly with conditions on pipe line specifications but is typically of the order of 6.4 x 10⁻⁵ kg/mmscm of gas. This corresponds to a water dew point at 70Bg of -7 °C, well below the hydrate formation point.

In order to assess the absorption duty between these
15 low concentrations, the thermodynamic equilibrium data - concentration of water in the gas, y^* , and concentration of water in the liquid phase, x - is required. Note:-

$$y^*_p = f(x)_p \quad (1)$$

20

i.e., the function f is dependent on the pressure. The relevant data shows that the separation can be achieved in one theoretical stage, i.e. if equilibrium were achieved in the contacting (mixing) process, then one
25 contact between the gas and liquid should give the required duty of water removal from the gas.

However, in conventional countercurrent tower units, 4 actual stages are normally specified. Stage efficiencies greater than 50% are simply not achieved.

30

It is therefore an object of the invention to provide a method and apparatus which enables water vapour to be removed from a natural gas with greater efficiency.

According to the invention, there is provided a method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

While the invention has been described in relation to natural gas, it is equally applicable to other gases with a water content which it is desirable to reduce.

The invention also extends to the apparatus for carrying out this method.

The turbulent mixing is very intense and results in extremely efficient gas liquid contact. The mixing regime is preferably turbulent shear layer mixing. The liquid entrained in the gas may be in the form of droplets for gas continuous fluid phase distribution. The efficient mixing means that absorption can take place very rapidly and in a relatively small total volume of absorbent compared to that required in conventional absorption columns. The mixing system used is simple and inexpensive compared to prior art systems, leading to reduced costs. Finally, an efficiency of approaching 100% for the removal of water can be achieved for certain applications.

The advantages of such a mixer in relation to conventional countercurrent dehydration towers are a reduction in the size and weight of the equipment.

Preferably, the method is carried out as a continuous process with the natural gas and liquid flowing co-currently. The co-current flow reduces the problems associated with foaming and flooding, since absorption can
5 continue downstream of the contactor.

One suitable contactor is a mixer supplied by Framo Engineering A/S and is described in EP-B-379319.

Preferably, the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the
10 outlet. In one possible regime, the natural gas is supplied to the tube, optionally directly, and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed. In another regime, the natural gas is supplied to
15 the vessel and the liquid is supplied to the tube, optionally directly, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed. In a third regime, the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above
20 the level of the outlet, whereby the natural gas is forced out through the outlet via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

Preferably, the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the
25 homogeneous mixtures optionally being cooled prior to separation into a gas phase and a liquid phase. Preferably, the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone. Preferably, the absorbent in the liquid phase is subjected to a
30 regeneration treatment to remove the absorbed water. Preferably, the regenerated absorbent-containing liquid phase is recycled to the contactor. Preferably, the regeneration is carried out by heating and/or by flashing off the water. Where the absorbent is a glycol,

regeneration may be carried out by heating the solution to about 200 °C and passing the vapours to a fractionating tower. Preferably, the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.

Partial recovery of the glycol may be attained by flashing off the water vapour by reducing the applied pressure on the liquid after gas dehydration. Where this is used then a similar turbulent mixer may be considered for this duty. This flashing operation will only give a partial glycol regeneration. In order to get to the very low levels of water content of the glycol solutions necessary for gas dehydration, heating of the solvent phase is required.

According to a more specific aspect of the invention, there is provided a method for removing water from a natural gas which comprises: supplying the natural gas to a turbulent contactor; supplying a liquid including an absorbent for the water to the contactor; subjecting the natural gas and the liquid to turbulent mixing in the contactor to form a homogeneous mixture; allowing the water to be absorbed by the absorbent; separating the homogeneous mixture into a gas phase and a liquid phase in a hydrocyclone (or any other gas/liquid separator); removing the gas phase; subjecting the solvent in the liquid phase to a regeneration treatment to remove the absorbed water; and recycling the regenerated absorbent-containing liquid phase to the contactor.

A portion of the solvent, after extraction may be recycled directed to the contactor.

Preferably, the absorbent includes a glycol or another water-miscible liquid. Preferably, the glycol is ethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these. The chosen absorbent could also be

immiscible with water and in this case, a facility for separating the water from the absorbent would need to be introduced downstream of the gas/liquid separator.

Diethylene glycol (DEG) and monoethylene glycol (MEG) are typical solvents for dehydration. Triethylene glycol (TEG) is currently the most popular solvent since it has a higher degradation temperature and can be regenerated to a higher lean concentration with no modification to a standard boiler. There has recently been a trend towards the reduction in BTEX (benzene, toluene, ethylbenzene, xylene) emissions which has in some cases favoured the use of MEG due to the much lower solubility of BTEX in this solvent. The penalty, however, is much higher glycol losses. The present invention envisages the use of any dehydration agent. However, the short residence time in the preferred contactor system (as compared with a counter-current absorption column) will necessarily result in less co-absorption of BTEX components in a given glycol system.

Preferably the natural gas and liquid are subjected to two or more mixing steps. Additional mixing steps may be carried out before and/or after the turbulent mixing step. One or more (or indeed all) of the additional mixing steps may themselves be turbulent mixing steps. They might be carried out using a similar turbulent contactor, or some other turbulent contactor, such as an ejector, a jet pump, or a mixer as described in WO 95/02448. Preferably, there are two or more turbulent mixing steps.

When second turbulent mixing is adopted, it is preferably conducted in a turbulent contactor comprising at least one fluid inlet, an outlet leading to a venturi passage, and a tube extending from the outlet back into the contactor. Preferably, the second contactor has a gas inlet and a liquid inlet. The tube may or may not be perforated, and the gap between the tube and the outlet may

be varied. Preferably, the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor. The second turbulent contactor may also have a separate liquid inlet for the addition of fresh
5 absorbent.

The invention also extends to apparatus for carrying out such a method, comprising: a turbulent contactor having a liquid inlet, a gas inlet and a fluid outlet; an optional cooler for the fluid stream from the fluid outlet; a
10 hydrocyclone arranged to separate the fluid stream into a gas phase and a liquid stream; a regenerator arranged to treat the separated liquid stream; and a recycle line arranged to convey the regenerated liquid stream to the contactor.

The apparatus may include a recycle line for the liquid stream from the separator to the contactor, by-passing the regenerator. There may also be a further separator, for example, in the form of a flash tank, in the
15 recycle line to allow absorbed water to be released from the liquid.
20

The apparatus may include a pump arranged to supply liquid to the liquid inlet of the contactor. Preferably, the regenerator is a heater and/or a flash tank.

The invention may be considered to extend to the use
25 of a turbulent contactor to remove water from natural gas by forming a homogeneous mixture of the gas mixture with an absorbent for the water in the contactor, allowing the water to be absorbed by the absorbent, and subsequently separating a gas phase and a liquid phase, the liquid phase
30 thereby containing the water.

The invention may be put into practice in various ways and some embodiments will be described by way of example to illustrate the invention with reference to the accompanying drawings, in which:

Figure 1 is a flow diagram of a process in accordance with the invention;

Figure 2 is a view of the contacting section of the apparatus; and

5 Figure 3 is a view of the glycol separation and regeneration sections.

Figure 1 shows a process for removing water from a gas stream, in accordance with the invention. The process comprises a turbulent contactor stage 11, a gas liquid
10 separator 12, a depressurizer 13 and a glycol regeneration stage 14. Water-bearing natural gas is fed to the contactor at 15 and a triethylene glycol (TEG) absorbent at 16. In the contactor 11, the TEG absorbs the water from the natural gas and a homogeneous gas/liquid mixture leaves
15 the contactor at 17.

The mixture is conveyed via line 18 to the separator 12 where the gas and liquid phases are separated. A water-free gas phase leaves the separator 12 at 19 and a liquid phase, comprising TEG and absorbed water is removed at 21.

20 This liquid phase is conveyed via a line 22 to a depressuriser 13 where water vapour is flashed off and removed via a water vapour outlet 23. The TEG with the remaining water is conveyed via a line 24 to the glycol regeneration stage 14, from which glycol is removed via a
25 glycol outlet 25 and water is removed via a water outlet 26. The regenerated glycol can be recycled to the glycol inlet 16 to the contactor stage 11.

The contactor stage 11 is shown in more detail in Figure 2. This stage 11 comprises two stages. The
30 turbulent contactor 100 forming the first stage comprises a vessel 101 having the natural gas inlet 15, the glycol inlet 16 and an outlet 104 leading to a venturi passage 105. There is a tube 106 (which may or may not be perforated) extending from the outlet 104 back into the

vessel 101.

The glycol and the natural gas are supplied to the vessel 101, the glycol being supplied to a level above the level of the outlet 104, whereby the gas is forced out through the outlet 104 via the tube 106, thereby drawing the glycol into the venturi so that the two phases are mixed.

The homogeneous gas/liquid mixture from the first turbulent contactor 100 is conveyed to a second turbulent contactor 110. Thus, the mixture enters an annular flow generator 150 from a spool piece 151, or directly from the diffuser of the venturi 105. As the gas/liquid mixture flows through the expanding outlet part of the annular flow generator 150, a liquid film establishes at the wall to form an annular gas/liquid flow essentially with the gas in the pipe core and the liquid at the pipe wall. The liquid film will be maintained in the annulus between inner and outer pipes 152 and 153 respectively.

The conditions at the outlet 154 of the inner pipe 152 are similar to the conditions at the outlet 104 of the first turbulent contactor. It is clear that, in principle, any number of stages can be added to the system, although considerations such as pressure drop should be taken into account.

As shown in Figure 2, the mixture leaving the second contactor 110 at the outlet 17 is conveyed to a hydrocyclone gas liquid separator 12 via a tangential inlet 31 (see Fig. 3). The two phases present are separated in the normal way. The gas phase, comprising dehydrated natural gas, passes upwards via a centre tube 32 and two demistor stages 33,34, and leaves via the gas outlet 19. The liquid phase, comprising glycol and absorbed water, passes downwards via a conical collector 35 and leaves via the liquid outlet 21. Accumulated liquid can be drained

from tubes at 37 at the level of the support ring for the centre tube 32.

5 The liquid is conveyed to a depressuriser 13, where some of the absorbed water is flashed off and leaves via the water vapour outlet 23. The glycol and any remaining absorbed water is pumped to the glycol regenerator 14 via the line 24. Here, the remaining absorbed water is separated from the glycol. The water is removed via the outlet 25 and dehydrated glycol is removed via the glycol outlet 26. This regenerated glycol is then recycled to the glycol inlet 16 to the contactor stage 11, via a recycle line 36.

10

Claims:

1. A method of removing water from natural gas which comprises: bringing the natural gas into contact with a liquid including an absorbent for the water; subjecting the natural gas and liquid to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the mixing is conducted in a turbulent contactor including a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.
2. A method as claimed Claim 1, in which the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet.
3. A method as claimed in Claim 2, in which the natural gas is supplied to the tube and the liquid is supplied to the vessel, and so the natural gas stream draws the liquid into the venturi and the two phases are mixed.
4. A method as claimed in Claim 2, in which the natural gas is supplied to the vessel and the liquid is supplied to the tube, whereby the natural gas is drawn into the venturi by the liquid and the two phases are mixed.
5. A method as claimed in Claim 2, in which the liquid and the natural gas are supplied to the vessel, the liquid being supplied to a level above the level of the outlet, whereby the natural gas is forced out through the outlet

via the tube, thereby drawing the liquid into the venturi so that the two phases are mixed.

5 6. A method as claimed in any preceding Claim, in which the method is carried out as a continuous process with the natural gas and liquid flowing co-currently.

10 7. A method as claimed in any preceding Claim, in which the natural gas and the liquid are formed into a homogeneous mixture in the contactor, the homogeneous mixture optionally being cooled prior to separation into a gas phase and a liquid phase.

15 8. A method as claimed in Claim 7, in which the homogeneous mixture is separated into a gas phase and a liquid phase in a hydrocyclone.

20 9. A method as claimed in any preceding Claim, in which the absorbent in the liquid phase is subjected to a regeneration treatment to remove the absorbed water.

25 10. A method as claimed in Claim 9, in which the regenerated absorbent-containing liquid phase is recycled to the contactor.

11. A method as claimed in Claim 10, in which the regeneration is carried out by heating and/or by flashing off the absorbed water.

30 12. A method as claimed in Claim 11, in which the post-mixing cooling and the regenerative heating are achieved, at least in part by mutual heat exchange.

13. A method as claimed in any preceding Claim, in which the absorbent is miscible with water.
14. A method as claimed in any of Claims 1 to 12, in which the absorbent is immiscible with water.
15. A method as claimed in any of Claims 1 to 12, in which the absorbent includes a glycol.
16. A method as claimed in Claim 15, in which the absorbent is monoethylene glycol, diethylene glycol, triethylene glycol or a mixture of any of these.
17. A method as claimed in any preceding Claim, in which the natural gas and liquid are subjected to two or more mixing steps.
18. A method as claimed in Claim 17, in which an additional mixing step is carried out before the turbulent mixing step.
19. A method as claimed in Claim 17 or Claim 18, in which an additional mixing step is carried out after the turbulent mixing step.
20. A method as claimed in Claim 18 or Claim 19 in which one or more additional mixing steps are turbulent mixing steps.
21. A method as claimed in Claim 20, in which the second mixing step is carried out in a second contactor, located in a pipe extending from the venturi passage of the first contactor.

22. A method as claimed in Claim 21, in which the fluid mixture is separated into a gas phase and a liquid phase between the two contactors, the phase separation preferably occurring in an annular flow generator.

5

23. A method as claimed in any of Claims 17 to 22, in which fresh liquid solvent is added to the second contactor.

10

24. Apparatus for removing water from natural gas by bringing the natural gas into contact with a liquid including an absorbent for the water, comprising: a turbulent contactor in which the natural gas and liquid are subjected to turbulent mixing conditions thereby causing the water to be absorbed by the absorbent; and a separator for separating a natural gas phase with reduced water content and a liquid phase including the absorbent and absorbed water; and in which the turbulent contactor comprises a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream, the tube being perforated and/or being spaced from the periphery of the outlet.

15

20

25. Apparatus as claimed Claim 24, in which the tube is located in a vessel, the vessel including the gas inlet, the liquid inlet and the outlet.

25

26. Apparatus as claimed in Claim 24 or Claim 25, in which the separator includes a hydrocyclone.

30

27. Apparatus as claimed in any of Claims 24 to 26, in which the separator includes an absorbent regenerator.

28. Apparatus as claimed in any of Claims 24 to 27, in which the contactor includes two or more contactor steps.

5 29. Apparatus as claimed in Claim 28, in which the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor.

10 30. The use of one or more turbulent contactor for absorbing water from a natural gas stream, in which the gas stream is brought into contact with a liquid including an absorbent for water, at least one of the turbulent contactors comprising a gas inlet, a liquid inlet, an outlet leading to a venturi passage and a tube extending from the outlet back upstream.

15

31. A use as claimed in Claim 30, in which the second turbulent contactor is located in a pipe extending from the venturi section of the first contactor.

20

32. A use as claimed in Claim 30 or Claim 31, in which a gas phase and a liquid phase are separated after exit from a first turbulent contactor before entry into a second turbulent contactor, the phase separation preferably occurring in an annular flow generator.

09/937241

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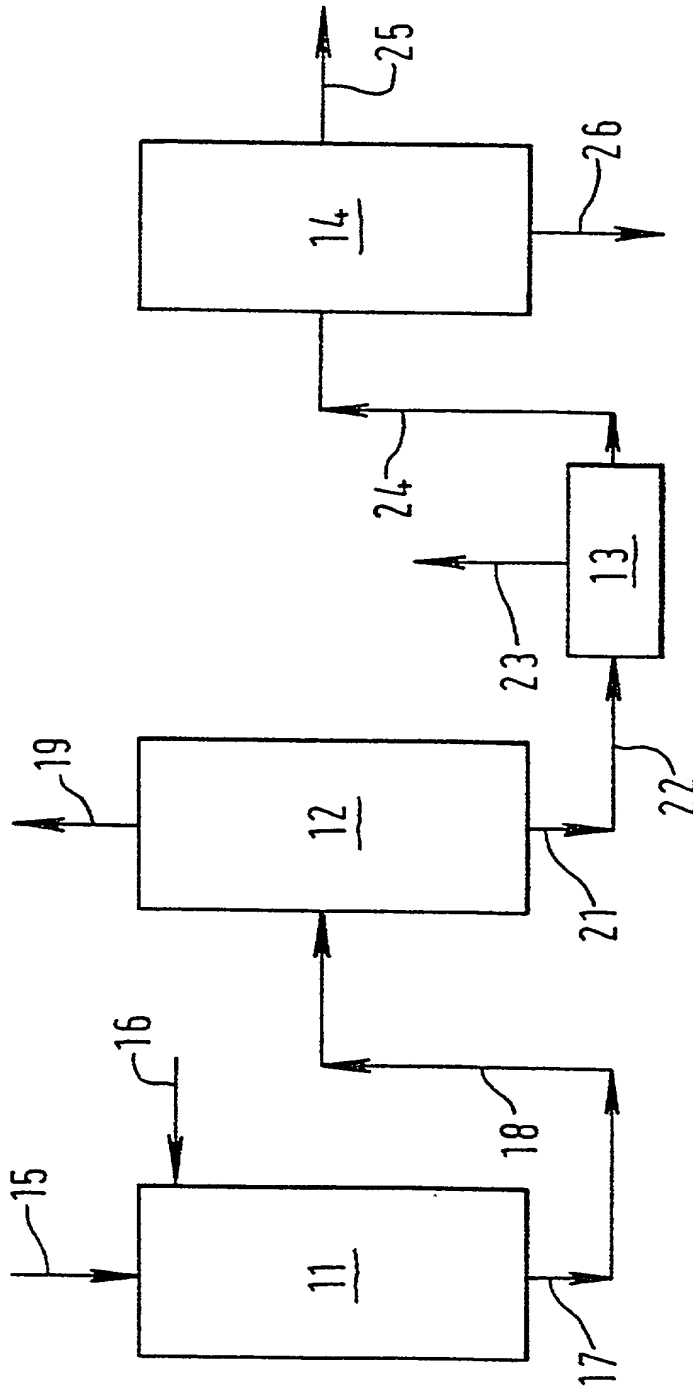
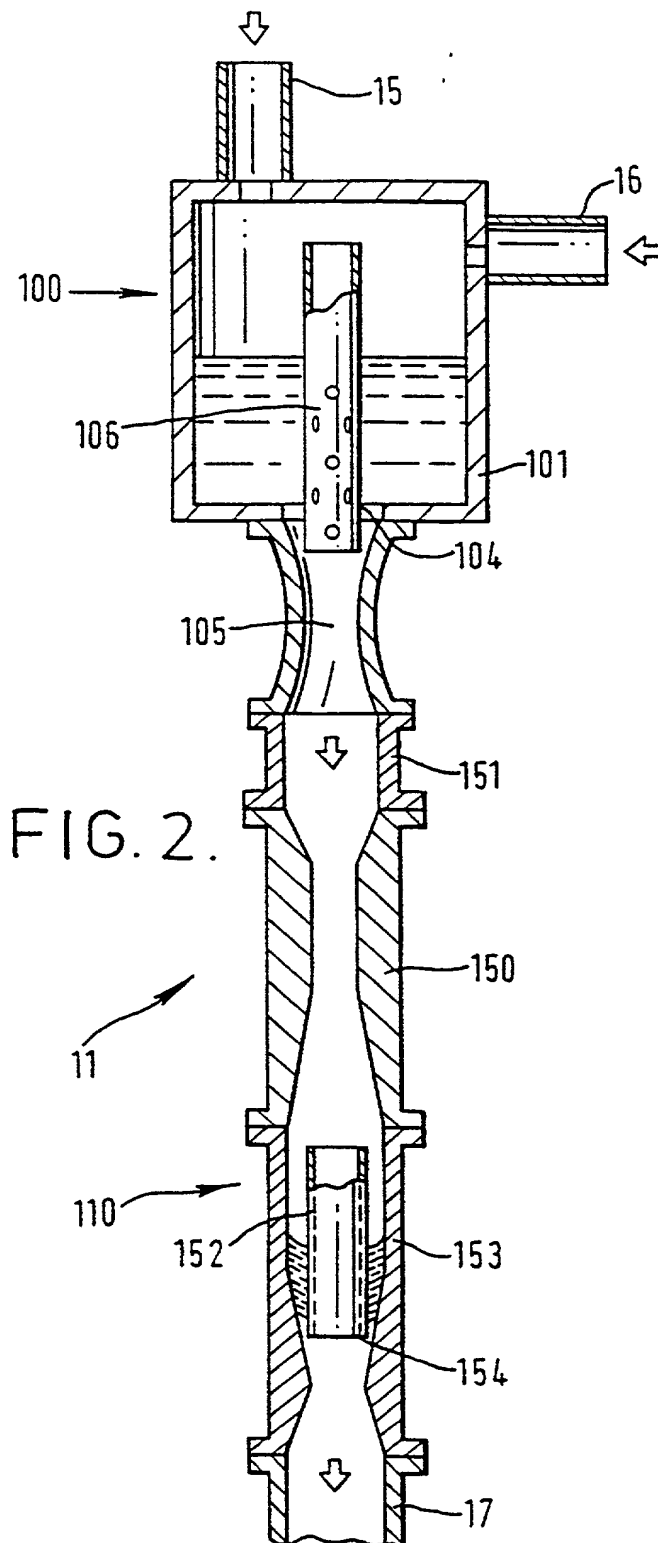


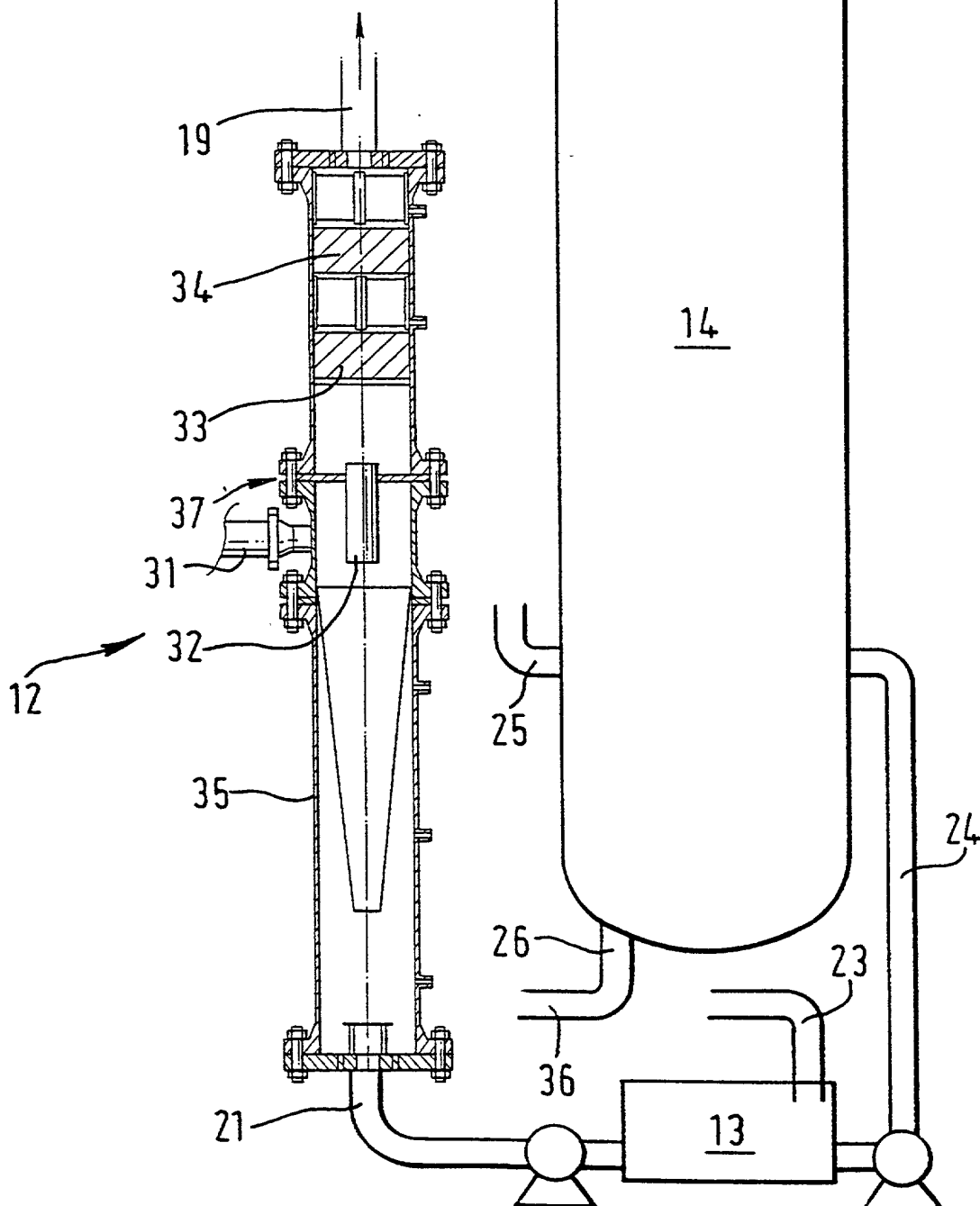
FIG.1.

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FIG. 3.



COMBINED DECLARATION AND POWER OF ATTORNEY

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled METHOD AND APPARATUS FOR THE DRYING OF NATURAL GAS, the specification of which is attached hereto unless the following is checked:

[X] The specification was filed on September 21, 2001 as United States Application Number or PCT International Application Number 09/937,241 and was amended on _____ (if applicable).

I hereby state that I have reviewed and understand the contents of the above-identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in Title 37, Code of Federal Regulations, § 1.56.

I hereby claim foreign priority benefits under Title 35, United States Code, § 119(a)-(d) of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed.

Prior Foreign Application(s)		Priority Claimed	
PCT/GB00/01070	WO	21 March 2000	Yes
(Number)	(Country)	(Day/Month/Year Filed)	(Yes/No)
9906717.5	GB	23 March 1999	Yes
(Number)	(Country)	(Day/Month/Year Filed)	(Yes/No)

I hereby claim the benefit under Title 35, United States Code, § 119(e) of any United States provisional application(s) listed below.

_____	_____
(Application Number)	(Filing Date)

_____	_____
(Application Number)	(Filing Date)

I hereby claim the benefit under Title 35, United States Code, § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application(s) in the manner provided by the first paragraph of Title 35, United States Code, § 112, I acknowledge the duty to disclose information which is material to patentability as defined in Title 37, Code of Federal Regulations, § 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application.

(Application Number) (Filing Date) (Status - patented, pending, abandoned)

(Application Number) (Filing Date) (Status - patented, pending, abandoned)

I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith:

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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